CLAIMS

What is claimed is:

- 1. A natural gas liquid plant, comprising:
 - a separator that separates a cooled low pressure feed gas into a liquid portion and a varpor portion, wherein the liquid portion is reduced in pressure in a first pressure reduction device, thereby providing refrigeration for a first cooler that cools a low pressure feed gas to form the cooled low pressure feed gas;
 - wherein at least part of the vapor portion is cooled in a second cooler and reduced in pressure in a second pressure reduction device before entering an absorber as lean absorber reflux; and
 - wherein the absorber produces an absorber overhead product that provides refrigeration for the second cooler, and wherein the absorber produces an absorber bottoms product that is fed into a demethanizer as lean reflux.
- 2. The natural gas liquid plant of claim 1 wherein the low pressure feed gas has a pressure of about 300 psig to about 1 000 psig.
- 3. The natural gas liquid plant of claim 1 wherein a portion of the low pressure feed is cooled in a plurality of side reboilers that are thermally coupled to the demethanizer.
- 4. The natural gas liquid plant of claim 1 wherein the first pres sure reduction device comprises a hydraulic turbine, and wherein the second press ure reduction device comprises a Joule-Thompson valve.
- 5. The natural gas liquid plant of claim 1 wherein the liquid portion that is reduced in pressure is fed into the demethanizer.
- 6. The natural gas liquid plant of claim 1 wherein part of the vapor portion is expanded in a turboexpander and fed into a second separator that produces a liquid that is employed as a lean demethanizer reflux and a vapor that is fed into the absorber.
- 7. The natural gas liquid plant of claim 1 wherein ethane recovery is at least 85 mol% and propage recovery is at least 99 mol%.

8. The natural gas liquid plant of claim 1 where in the first and second coolers and the absorber are installed as an upgrade to an existing plant.

- 9. A natural gas liquid plant, comprising:
 - a primary and secondary cooler that cool a low pressure feed gas, and a separator that separates the cooled low pressure feed gas in a liquid portion and a vapor portion;
 - a first pressure reduction device that reduces pressure of the liquid portion, thereby providing refrigeration for the second ary cooler;
 - a third cooler that cools at least part of the varpor portion, wherein the cooled vapor portion is expanded in a pressure reduction device; and
 - an absorber that receives the cooled and expanded vapor portion and produces an overhead product that provides refrigeration for the third cooler and a bottom product that is employed as reflux in a demethanizer.
- 10. The natural gas liquid plant of claim 9 wherein the low pressure feed gas is at least partially dehydrated and has a pressure of between about 300 psig and about 1000 psig.
- 11. The natural gas liquid plant of claim 9 wherein the first pressure reduction device comprises a hydraulic turbine and wherein the second pressure reduction device comprises a Joule-Thompson valve.
- 12. The natural gas liquid plant of claim 9 wherein a portion of the low pressure feed gas is cooled in a plurality of side reboilers that are thermally coupled to the demethanizer.
- 13. The natural gas liquid plant of claim 9 whereim part of the vapor portion is expanded in a turboexpander and fed into a second separator that produces a liquid that is employed as a lean demethanizer reflux and a vapor that is fed into the absorber.
- 14. The natural gas liquid plant of claim 9 wherein the primary cooler employs as least one of external ethane, external propane, and the absorber overhead product as a refrigerant.

15. The natural gas liquid plant of claim 9 wherein ethane recovery is at least 85 mol % and propane recovery is at least 99 mol%.

- 16. A natural gas liquid plant comprising a separator receiving a cooled low pressure feed gas and fluidly coupled to an absorber and a demethanizer, wherein refrigeration duty of the absorber and demethanizer are provided at least in part by expansion of a liquid portion of the cooled low pressure feed gas and an expansion of a vapor portion using a device other than a turboexpander.
- 17. The natural gas liquid plant of claim 16 wherein the cooled low pressure feed gas has been cooled by a cooler that employs an expanded liquid portion of the cooled low pressure feed gas as s refrigerant.
- 18. The natural gas liquid plant of claim 16 wherein the absorber produces an absorber bottom product that is fed to the demethanizer as reflux.
- 19. The natural gas liquid plant of claim 16 wherein the separator separates a vapor portion from the cooled low pressure feed gas and wherein a first part of the vapor portion is further cooled via a joule-Thompson valve and introduced into the absorber.
- 20. The natural gas liquid plant of claim 19 wherein a second part of the vapor portion is expanded and cooled in a turboexpander.

AMENDED CLAIMS

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What is claimed is:

- 1. A natural gas liquid plant, comprising:
 - a separator that separates a cooled low pressure feed gas into a liquid portion and a vapor portion, wherein the liquid portion is reduced in pressure in a first pressure reduction device, thereby providing refriger ation for a first cooler that cools a low pressure feed gas thereby forming the cooled low pressure feed gas;
 - wherein at least part of the vapor portion is cooled in a second cooler and reduced impressure in a second pressure reduction device before entering an absorber as lean absorber reflux; and
 - wherein the absorber produces an absorber overhead producet that provides refrigeration for the second cooler, and wherein the absorber produces an absorber bottoms product that is fed into a demethan izer as lean reflux.
- 2. The natural gas liquid plant of claim 1 wherein the low pressure feed gas has a pressure of about 300 psig to about 1000 psig.
- 3. The natural gas liquid plant of claim 1 wherein a portion of the low pressure feed is cooled in a plurality of side reboilers that are thermally coupled to the demethanizer.
- 4. The natural gas liquid plant of claim 1 wherein the first pres sure reduction device comprises a hydraulic turbine, and wherein the second pressure reduction device comprises a Joule-Thompson valve.
- 5. The natural gas liquid plant of claim 1 wherein the liquid portion that is reduced in pressure is fed into the demethanizer.
- 6. The natural gas liquid plant of claim 1 wherein part of the vapor portion is expanded in a turbo expander and fed into a second separator that produces a liquid that is employed as a lean demethanizer reflux and a vapor that is fed into the absorber.

7. The natural gas liquid plant of claim 1 wherein ethane recovery is at least 85 mol% and propane recovery is at least 99 mol%.

- 8. The natural gas liquid plant of claim 1 wherein the first and second coolers and the absorber are installed as an upgrade to an existing plant.
- 9. A natural gas liquid plant, comprising:
 - a primary and secondary cooler that cool a Low pressure feed gas, and a separator that separates the cooled low pressure feed gas in a liquid portion and a vapor portion;
 - a first pressure reduction device that reduces pressure of the liquid portion and thereby provides refrigeration for the secondary cooler;
 - a third cooler that cools at least part of the vapor portion, wherein the cooled vapor portion is expanded in a pressure reduction device; and
 - an absorber that receives the cooled and expanded vapor portion and produces an overhead product that provides refrigeration for the third cooler and a bottom product that is employed as reflux in a demethanizer.
- 10. The natural gas liquid plant of claim 9 wherein the low pressure feed gas is at least partially dehydrated and has a pressure of between about 300 psig and about 1000 psig.
- 11. The natural gas liquid plant of claim 9 wherein the first pressure reduction device comprises a hydraulic turbine and wherein the second pressure reduction device comprises a Joule-Thompson valve.
- 12. The natural gas liquid plant of claim 9 wherein a portion of the low pressure feed gas is cooled in a plurality of side reboilers that are thermally coupled to the demethanizer.
- 13. The natural gas liquid plant of claim 9 wherein part of the vapor portion is expanded in a turboexpander and fed into a second separator that produces a Liquid that is employed as a learn demethanizer reflux and a vapor that is fed into the absorber.

14. The natural gas liquid plant of claim 9 wherein the primary cooler employs as least one of external ethane, external propane, and the absorber overhead product as a refrigerant.

- 15. The natural gas liquid plant of claim 9 wherein ethanne recovery is at least 85 mol% and propane recovery is at least 99 mol%.
- 16. A matural gas liquid plant that comprises a separator receiving a cooled low pressure feed gas and fluidly coupled to an absorber and a demethanizer, wherein refri geration duty of the absorber and demethanizer are provided at least in part by expansion of a liquid portion of the cooled low pressure feed gas and an expansion of a vapor portion using a device other than a turboexpander.
- 17. The natural gas liquid plant of claim 16 wherein the cooled low pressure feed gas has been cooled by a cooler that employs an expanded liquid portion of the cooled low pressure feed gas as s refrigerant.
- 18. The natural gas liquid plant of claim 16 wherein the absorber produces an absorber bottom product that is fed to the demethanizer as reflux.
 - 19. The natural gas liquid plant of claim 16 wherein the separator separates a vap or portion from the cooled low pressure feed gas and wherein a first part of the vapor portion is further cooled via a joule-Thompson valve and introduced into the absorber.
- 20. The natural gas liquid plant of claim 19 wherein a second part of the vapor portion is expanded and cooled in a turboexpander.